

IN THE CLAIMS

Please amend the claims as follows:

1. (currently amended): A fixed-bed multitubular reactor, comprising:  
a plurality of reaction tubes to be packed with a catalyst;  
catalyst temperature measures equipped to measure the temperature near the centre  
part in the radial direction of the reaction tubes;  
a heat-medium bath located outside of said reaction tubes;  
heat-medium bath temperature measures measuring temperatures of said heat-  
medium;  
at least a portion of said plurality of reaction tubes being arranged so as to be adjacent  
to each other to form at least one reaction tube group; ~~and~~  
wherein the catalyst temperature measures being installed in all of the plurality of  
the reaction tubes or at least a part of said reaction tubes forming said at least one reaction  
tube group, the measurement positions thereof being different from each other in the  
longitudinal direction of the reaction tubes; and  
the heat-medium bath temperature measures are equipped corresponding to the  
catalyst temperature measures so that the measurement positions Q thereof are set at the same  
height as the measurement positions P of the catalyst temperature measures.

2. (original) The fixed-bed multitubular reactor according to claim 1, wherein the  
catalyst temperature measurers are equipped in 5 to 35 tubes out of a reaction tube group  
comprising 5 to 105 reaction tubes adjacent to each other.

3. (previously presented): The fixed-bed multitubular reactor according to claim 2, wherein flow patterns of a heat medium are different in the reactor, and a plurality of the reaction tube groups are provided and respectively allocated to the positions where the flow patterns of the heat medium are different.

4. (currently amended): A ~~fixed-bed multitubular reactor which is used~~ method for conducting a gas-phase catalytic oxidation reaction, comprising:  
—— ~~a plurality of reaction tubes to be packed with a catalyst;~~  
—— ~~catalyst temperature measures equipped to measure the temperature near the centre part in the radial direction of the reaction tubes;~~  
—— ~~at least a portion of said plurality of reaction tubes are arranged so as to be adjacent to each other to form at least one reaction tube group; and~~  
  
the catalyst temperature measures being installed in all of the plurality of the reaction tubes or at least a part of said reaction tubes forming the reaction tube group, the measurement positions thereof being different from each other in the longitudinal direction of the reaction tubes oxidizing a gas in the fixed-bed multitubular reactor of claim 1.

5. (currently amended) The ~~fixed-bed multitubular reactor~~ method according to claim 4, wherein the gas-phase catalytic oxidation reaction is a reaction synthesizing an unsaturated aldehyde or an unsaturated carboxylic acid from propylene, isobutylene or tertiary butyl alcohol.

6. (currently amended) The ~~fixed-bed multitubular reactor~~ method according to claim 4, wherein the gas-phase catalytic oxidation reaction is a reaction synthesizing an unsaturated carboxylic acid from an unsaturated aldehyde.

7. (cancelled)

8. (previously presented): The fixed-bed multitubular reactor according to claim 1, wherein a plurality of the reaction tubes groups are allocated circularly and at least one reaction tube group is allocated in each section L which is made by separating the cross section of the reactor in the radial direction from the centre M into two or more sections having the same area.

9. (previously presented): The fixed-bed multitubular reactor according to claim 1, wherein the length of the reaction tube is 2 to 7 meters.

10. (previously presented): The fixed-bed multitubular reactor according to claim 1, wherein the setting interval of the catalyst temperature measures is from 0.1 to 2 meters.

11. (previously presented) The fixed-bed multitubular reactor according to claim 1, comprising a plurality of reaction tube groups arranged in a triangular configuration.

12. (previously presented) The fixed-bed multitubular reactor according to claim 1, comprising a plurality of reaction tube groups arranged in a square configuration.